



FLORIDA ONSITE SEWAGE NITROGEN REDUCTION STRATEGIES (FOSNRS) STUDY

Presentation to the FDOH Research Review and Advisory Committee (RRAC) July 28, 2015

ADENT PORT

OTIS ENVIRONMENTAI CONSULTANTS

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PROJECT TEAM ACKNOWLEDGEMENTS











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And many support firms and staff! Special acknowledgements to the volunteer homeowners!

Presentation Outline

- Excess Nitrogen impacts water quality!
- Florida onsite sewage nitrogen reduction strategies (FOSNRS) project background
- Task A: Technology Review and Pilot Testing
- Task B: Full Scale Prototype PNRS Testing
 - Proprietary system (System 1)
 - In-tank PNRS (System 2)
 - In-ground PNRS (System 3)
- Task C: Soil and Groundwater Monitoring
- Task D: Nitrogen Fate & Transport Modeling and Tool Development
- Summary & Questions





Why are we here?

Excess Nitrogen impacts water quality!

Adverse effects of nitrogen

- Public Health: SDWA Limit of 10 mg/L NO₃ N, Harmful Algal Blooms (HABs)
- Ecosystem Health/ Water Qualty: N is limiting nutrient in many water bodies
 - Algal blooms, loss of habitat, hypoxia
- Impacts of excess nitrogen on water quality have been documented in many areas:
 - Tampa Bay, Sarasota Bay, Indian River Lagoon
 - Florida Keys
 - Florida's Freshwater Springs and elsewhere

In Florida, nitrogen loading has resulted in water quality problems for our freshwater springs...

Ichetucknee, Springs State Park, 1995

Ichetucknee Springs State Park, 2012

Photos courtesy of John Moran - SpringsEternalProject.org

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Nitrogen reducing onsite wastewater systems (OWS)

- Concerns over nitrogen impacts have led to requirements to reduce nitrogen, typically to a 10 mg/L total nitrogen goal prior to discharge to the soil
 - Florida Keys
 - Wakulla County, FL
 - Performance based treatment systems (PBTS) utilizing an activated sludge biological (BNR) process, similar to a municipal treatment plant, have been typically used.
 - Inconsistent performance of PBTS has been documented, with systems generally unable to meet 10 mg/L TN goal.



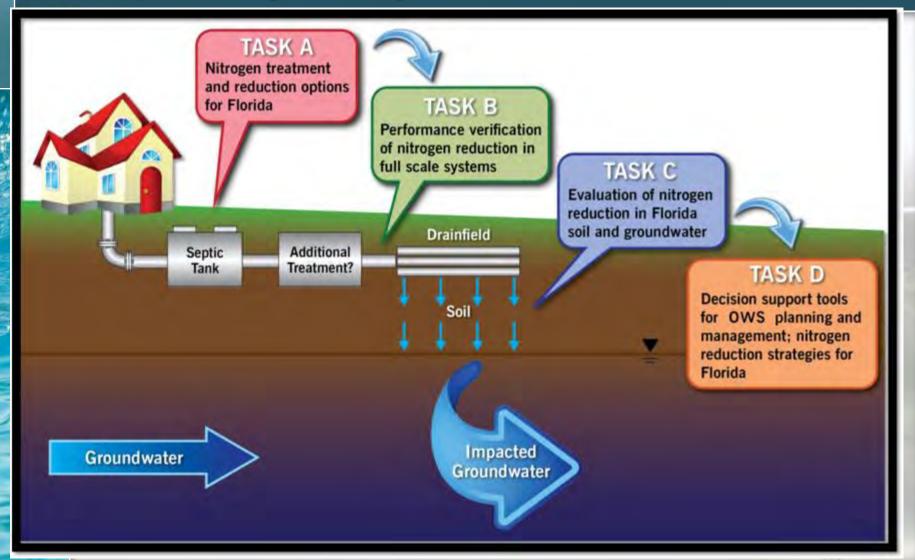


Florida Onsite Sewage Nitrogen Reduction Strategies (FOSNRS) project background

FOSNRS project initiated by Florida legislature

- Florida Legislature directed FDOH to conduct a study to further develop more "passive" & cost-effective nitrogen reduction strategies for onsite sewage treatment and disposal systems (OSTDS)
- "Passive" nitrogen reducing OSTDS should be more similar to conventional onsite systems in their operation and maintenance
 - Initiated the Florida Onsite Sewage Nitrogen Reduction Strategies (FOSNRS) Project in 2009
- RFP identified four primary study areas

Four primary study areas







Task A: Technology Review and Pilot Testing

Task A Components

- Literature review to evaluate nitrogen reducing technologies
- Ranking and prioritization of nitrogen reducing technologies for field testing
- Technology ranking workshop with RRAC conducted on May 28, 2009
- Pilot testing of passive nitrogen reduction systems (PNRS)
- Materials testing for FDOH additives rule

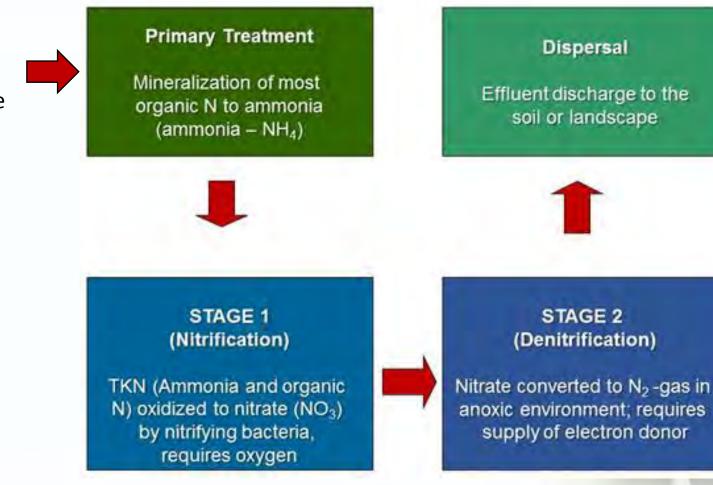
Treatment Technology Rankings

	System Rank	Technology/Process	Comments
	1	Two stage (segregated biomass) system: <i>Stage 1:</i> Biofiltration with recycle (nitrification) <i>Stage 2:</i> Autotrophic denitrification with reactive media biofilter	 Top ranked system capable of meeting the lowest TN concentration standard Suitable for new systems or retrofit
A DESCRIPTION OF A DESC	2	Two stage (segregated biomass) system: <i>Stage 1:</i> Biofiltration with recycle (nitrification) <i>Stage 2:</i> Heterotrophic denitrification with reactive media biofilter	 Top ranked system capable of meeting the lowest TN concentration standard Suitable for new systems or retrofit
	3	Natural system: Septic tank/STU (Drainfield) with in-situ reactive media layers, Stage 1 media over Stage 2 media	 Lower cost natural system that is untested but appears capable of achieving 75-78% TN removal before reaching groundwater Suitable for new systems or replacing existing systems at end of useful life

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Biological Nitrogen Removal (BNR) Two stage biofiltration is more stable process





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Unique pilot test facility was designed and constructed

- Follow up to PNRS I with larger, pilot scale units and various media combinations
- Established test facility at Gulf Coast Education and Research Center (University of Florida IFAS)
- Operated on septic tank effluent for 12+ months
- Produce scalable design criteria from pilot scale biofilters for subsequent full-scale testing



What are "passive" nitrogen reduction systems?

- Passive nitrogen reduction systems (PNRS) are OSTDS that reduce effluent N using reactive media for denitrification and a single liquid pump, if necessary.
 - Two stage process:
 - Stage 1: "nitrify" nitrogen compounds to NO₃ (nitrification)
 - Stage 2: "denitrify" NO₃ to nitrogen gas
 (denitrification)



nitrification media: sand & expanded clay



denitrification media: lignocellulosics



denitrification media: elemental sulfur

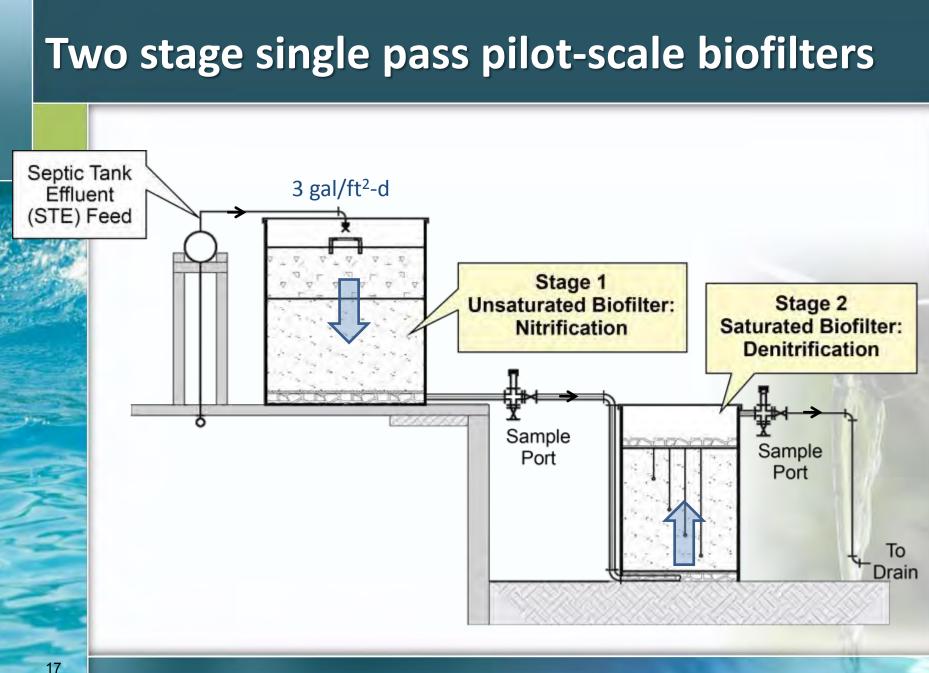
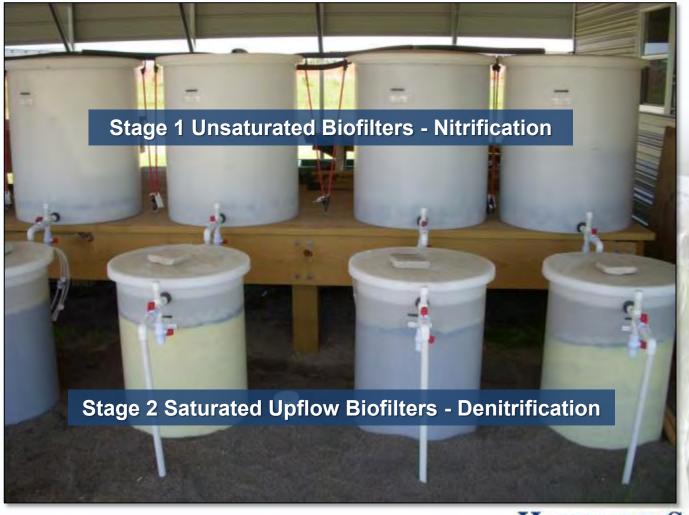


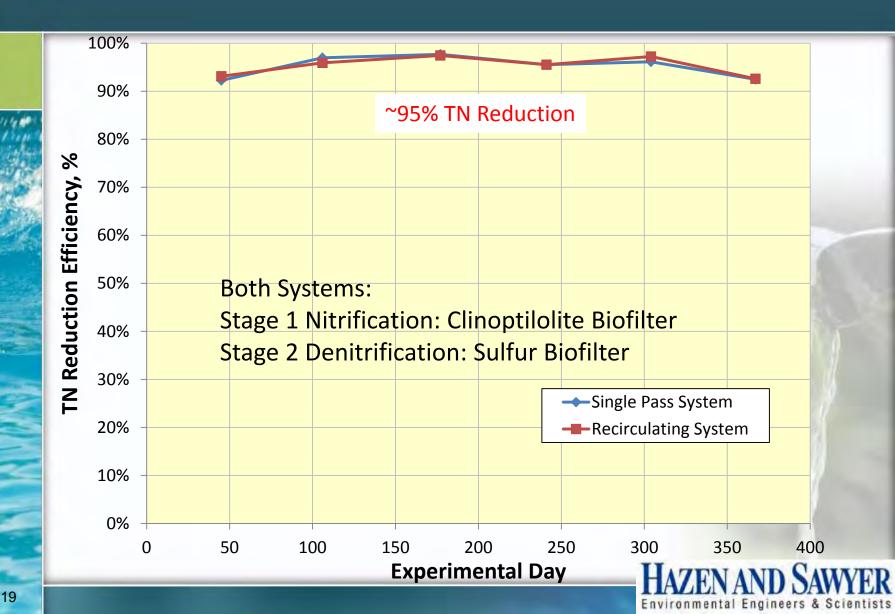
Photo of two-stage single pass biofilter pilot units



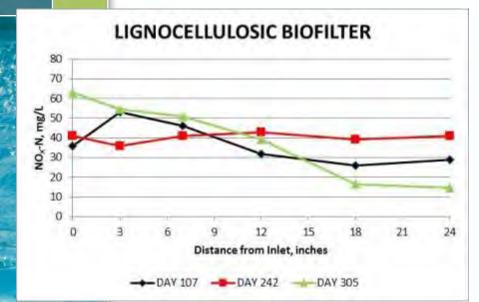


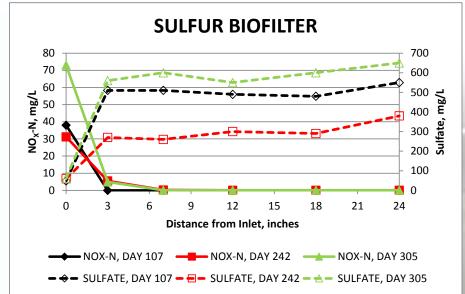
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PNRS pilot-scale test results



Vertical sampler profile in upflow biofilters



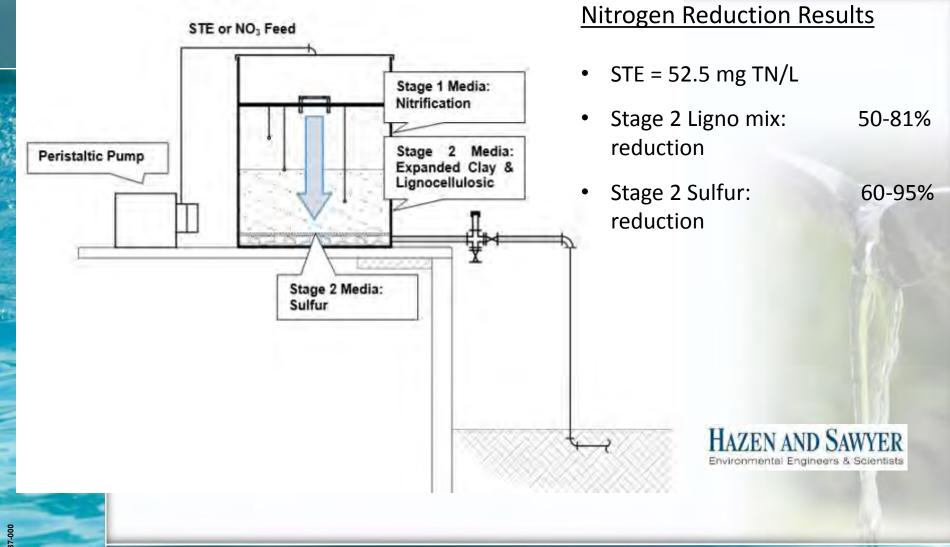




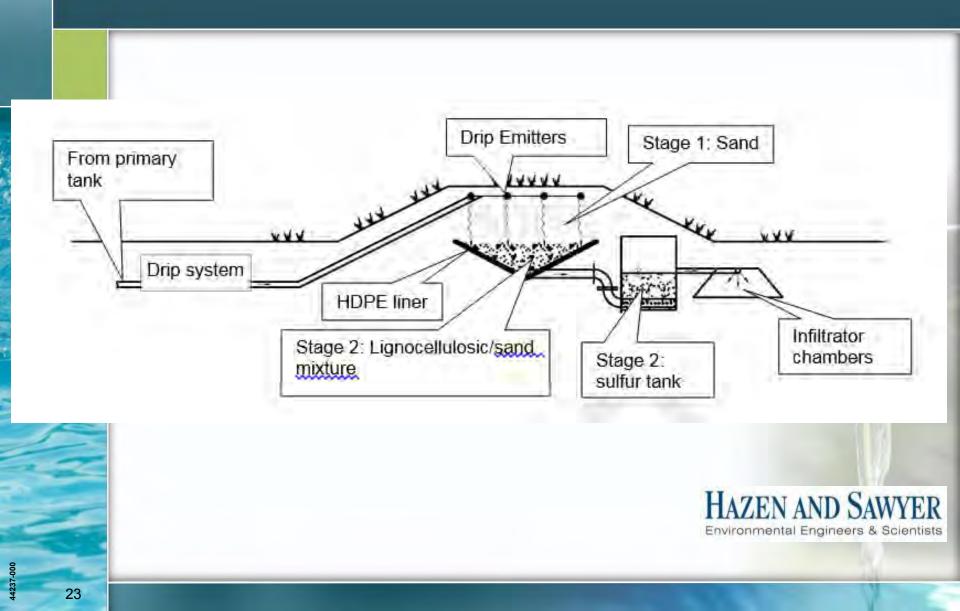
Development of in-ground PNRS concepts

- Tank based PNRS performed extremely well (previous talk), but large tankage requirements make systems expensive
- Desired an in-ground system that could be constructed like a soil treatment unit (drainfield)
- Conceptual ideas revolved around a vertically stacked PNRS, where Stage 1 media was placed over the Stage 2 media
- Liner could be used to saturate Stage 2 media and collect treated effluent

Vertically stacked Stage 1/Stage 2 concept was first pilot tested in small tanks



Successful pilot concept developed into prototype in-ground PNRS for further testing



Shaping soil for liner

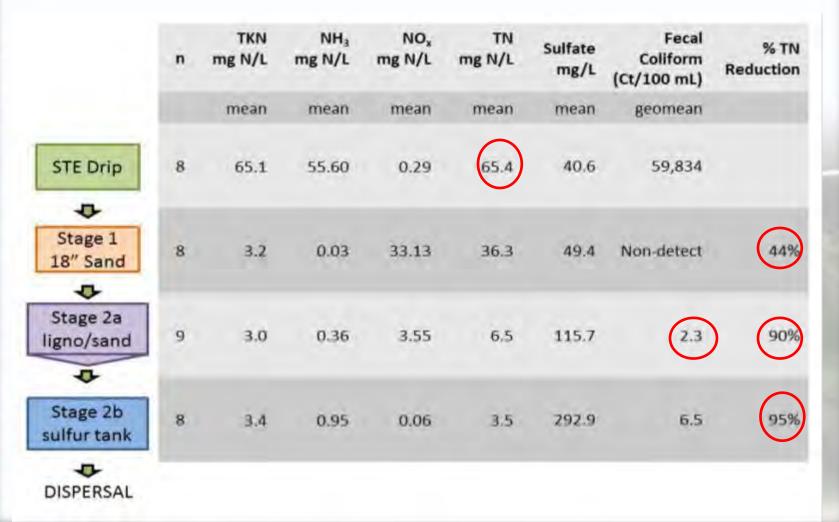






Prototype in-ground PNRS performance

Mean results over 8 sample events, 523 days of operation



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Lessons learned from pilot test

- Encouraging results from pilot PNRS; several system configurations capable of <u>></u> 95% N reduction
- Sulfate production vs nitrate reduction
- Highly reactive elemental sulfur media
- Lignocellulosic retention time issues
- Recommended evaluation of combination lignocellulosic and elemental sulfur denitrification systems for full-scale treatment units





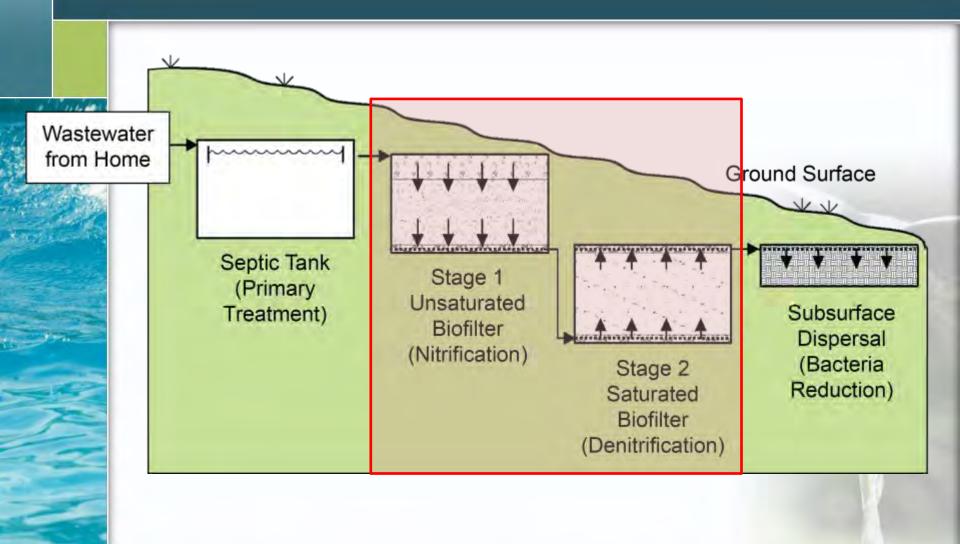
Task B: Full Scale Prototype PNRS Testing

Task B Components

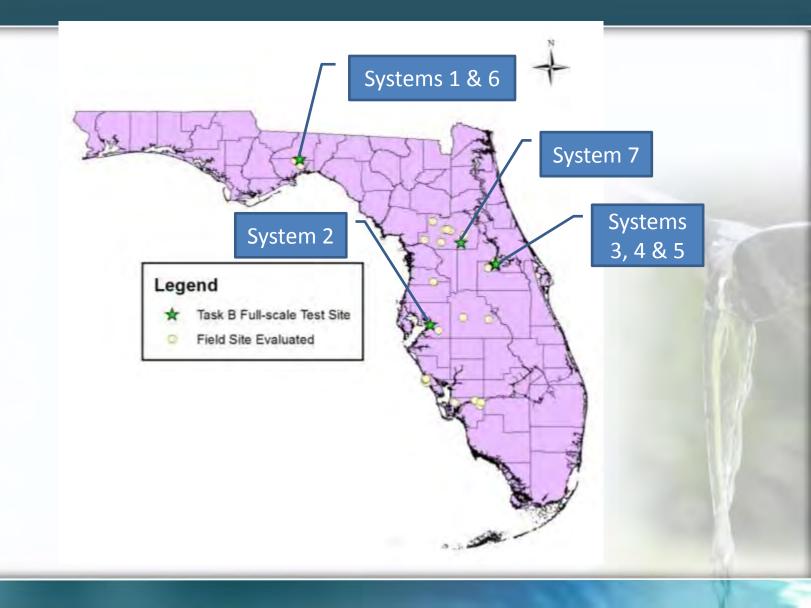
- Full scale operation and monitoring of 7 nitrogen reducing technologies at single family residences
- Developed PNRS Life Cycle Cost Analysis tool

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Task B: Full scale concepts complement existing OSTDS



Full scale PNRS installed



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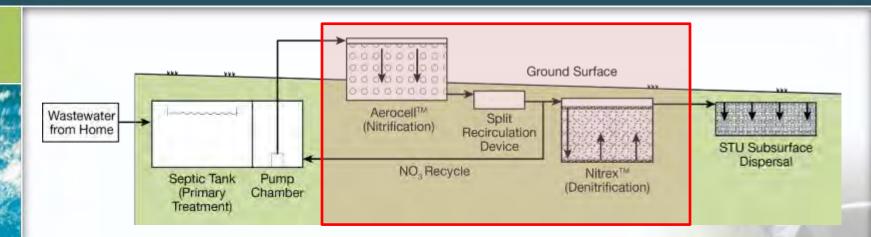
Full scale PNRS Summary

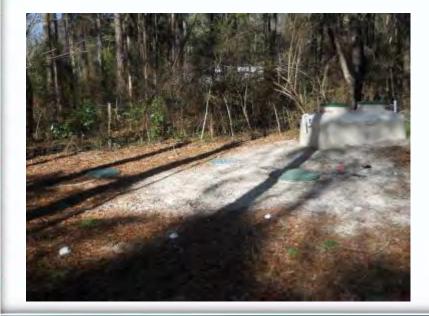
		Design	Location (County)	Stage 1 Hydraulics	Stage 2 Hydraulics
No. of Street, or other	System 1	Proprietary	Wakulla	Pumped with recirculation	Gravity
	System 2	In-tank PNRS	Hillsborough	Pumped with recirculation	Pumped
	System 3	In-ground PNRS	Seminole	Pumped with subsurface drip irrigation	Gravity
	System 4	In-tank PNRS	Seminole	Gravity	Gravity
1.1	System 5	In-tank PNRS	Seminole	Pumped single pass and tested with recirculation	Pumped
	System 6	In-tank PNRS	Wakulla	Pumped single pass vertically stacked	Gravity
00	System 7	In-ground PNRS	Marion	Pumped low pressure distribution	Gravity



Proprietary system (System 1)

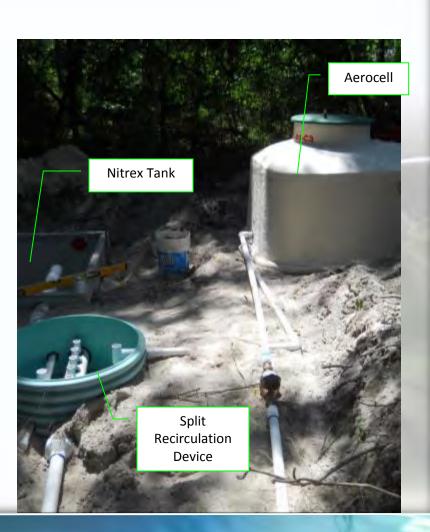
Proprietary System 1





- Single family home
- 3 bedroom
- 4 residents
- Flow of 112 gpd



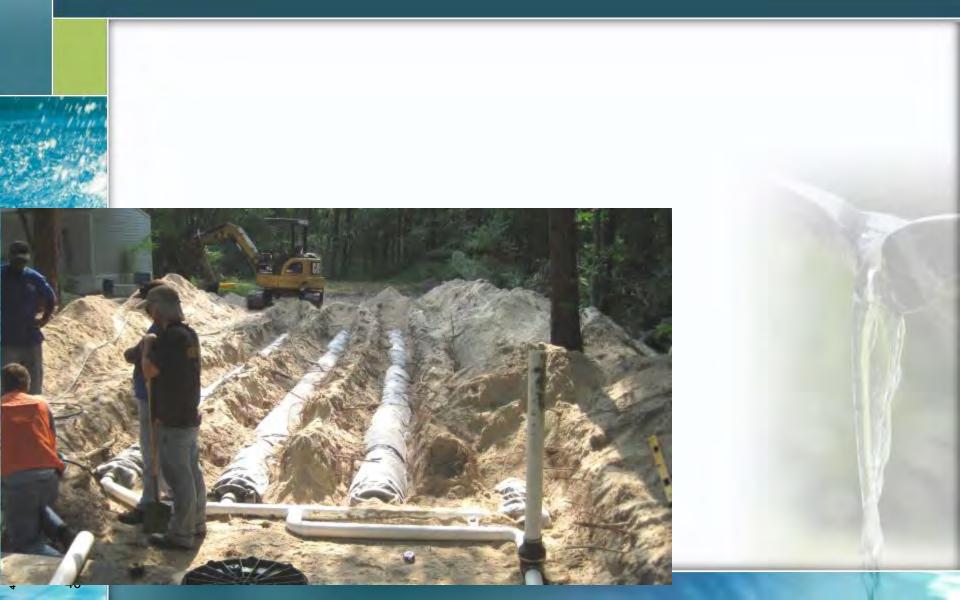


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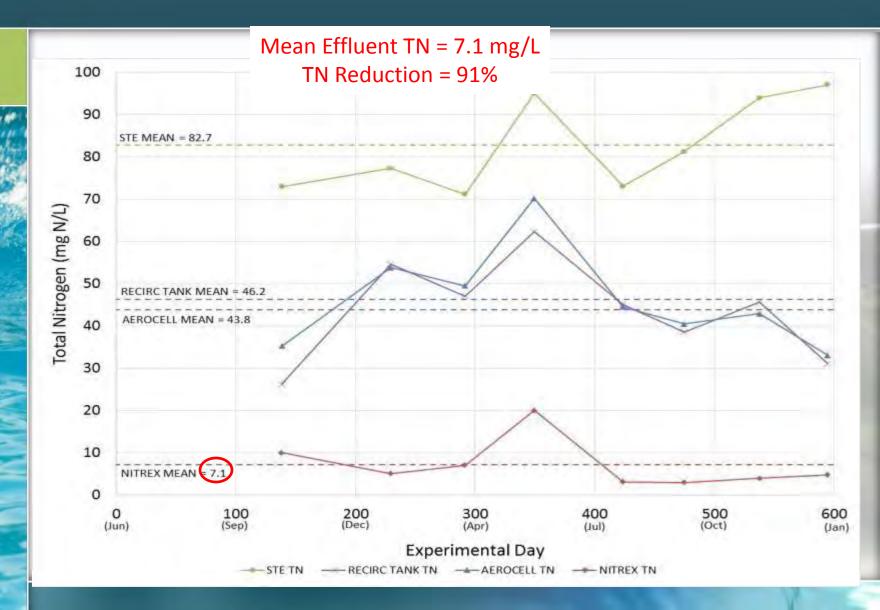








System 1 Time series of nitrogen data



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System 1: Operation and maintenance

- Average energy consumption of 3.21 kWh/day or 28.7 kWh/1000 gal treated (~\$120 per year)
- AerocellTM (Stage 1 biofilter) no surficial biomat or clogging present
- Nitrex[™] (Stage 2 biofilter) reactive media showed very little reduction in volume

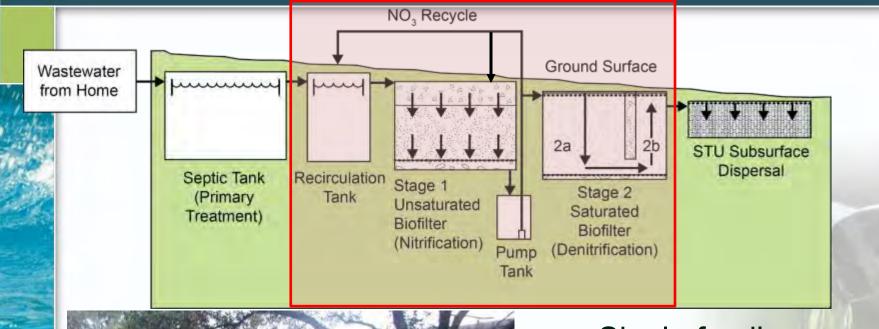






In-tank PNRS (System 2)

In-tank PNRS (System 2)





- Single family home
- 3 bedroom
- 2 residents
- Flow of 108 gpd

Stage 1 biofilter construction



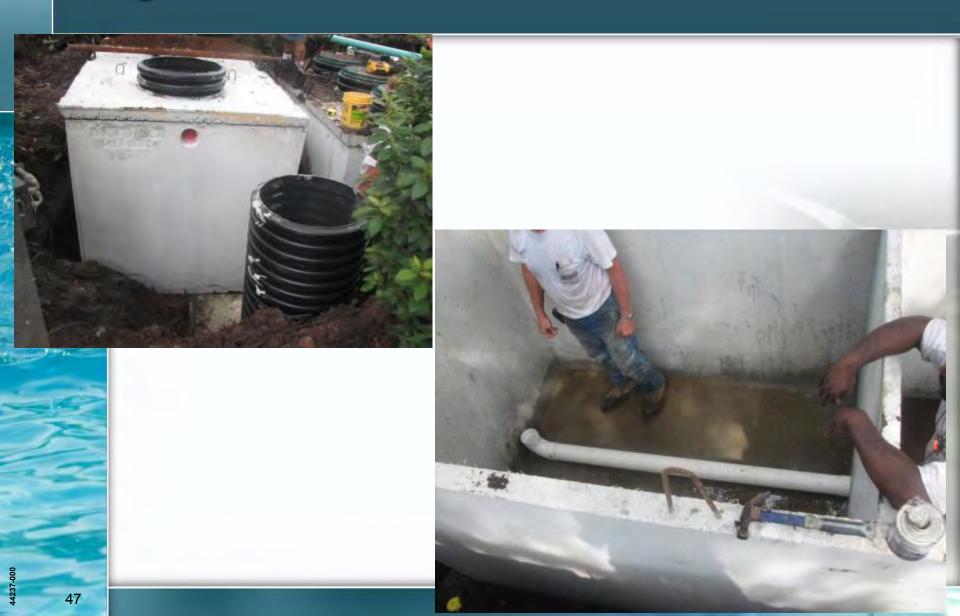
Stage 1 biofilter construction



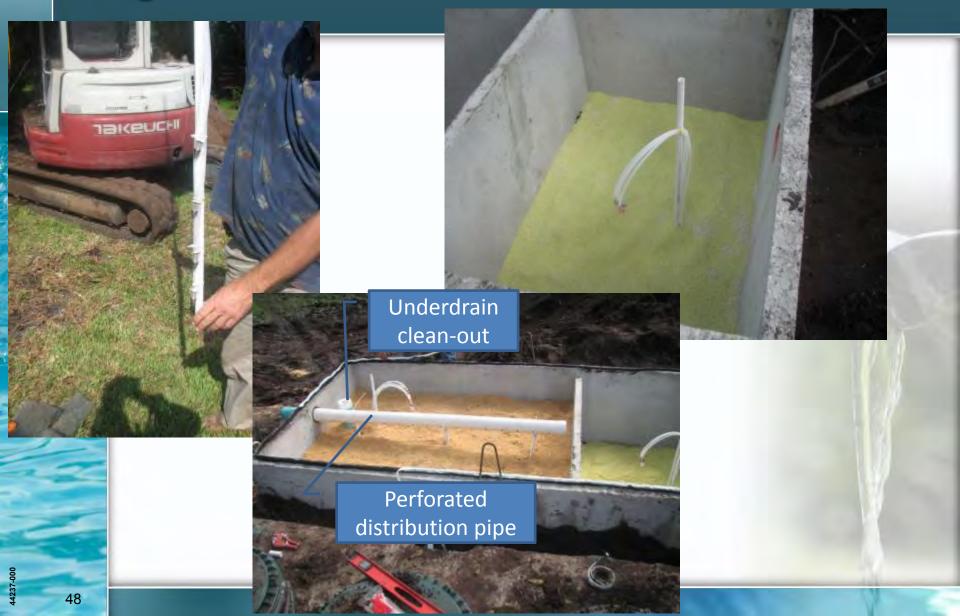


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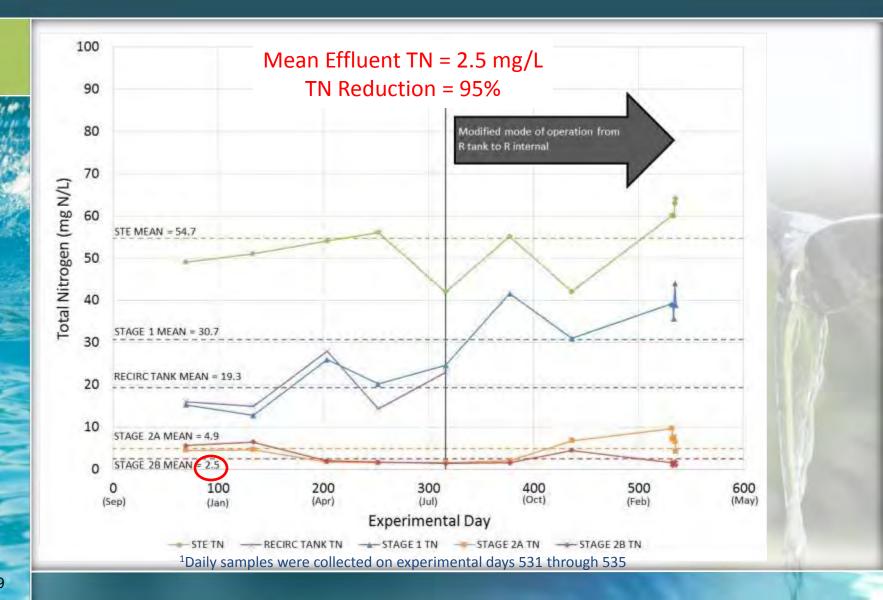
Stage 2 biofilter construction



Stage 2 biofilter construction



System 2 Time series of nitrogen data



System 2: Operation and maintenance

- Average energy consumption of 0.28 kWh/day or 2.6 kWh/1000 gal treated (~\$10 per year)
- Stage 1 biofilter no surficial biomat or clogging present
- Stage 2 biofilter reactive media showed very little reduction in volume

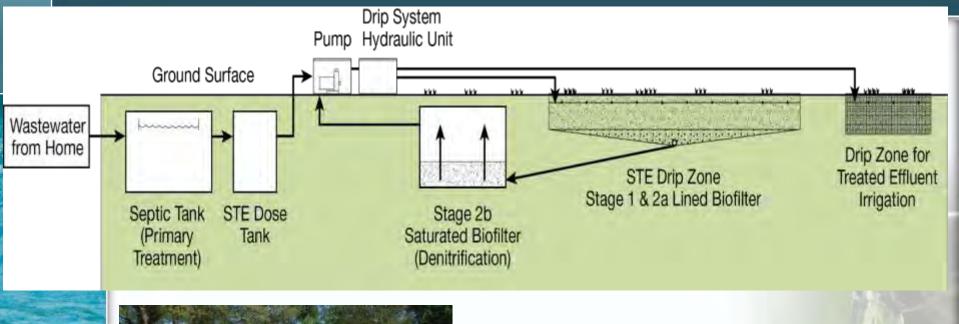






In-ground PNRS (System 3)

In-ground PNRS (System 3) with onsite reuse





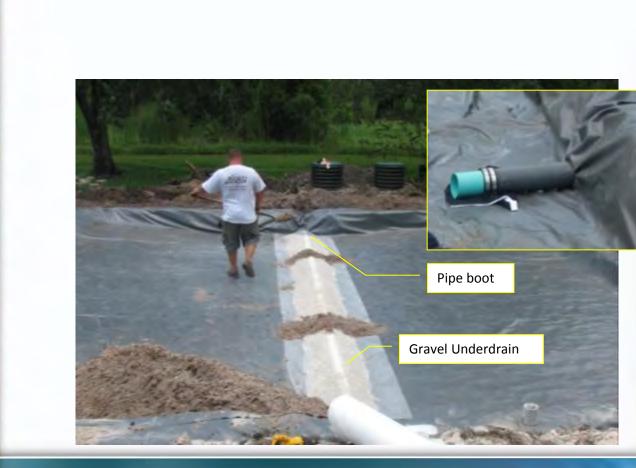
- 5 bedroom (2 residents)
- Flow of 145 gpd
- Mounded drainfield
- Soils: Myakka and EauGallie fine sands

Construction: Liner installation



>

Construction: Liner installation



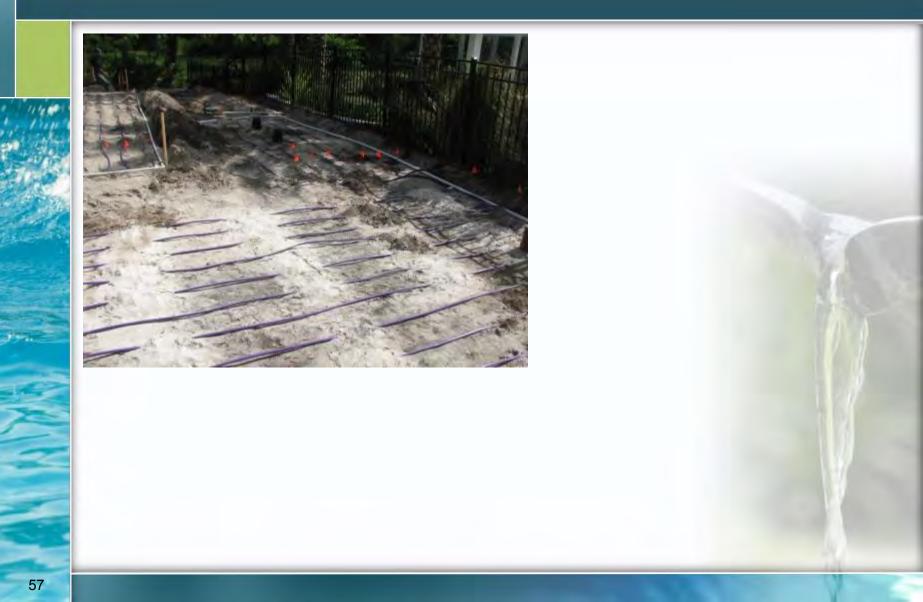
Stage 1 biofilter w drip irrigation of STE



Stage 2 sulfur biofilter construction



Subsurface drip irrigation of treated effluent

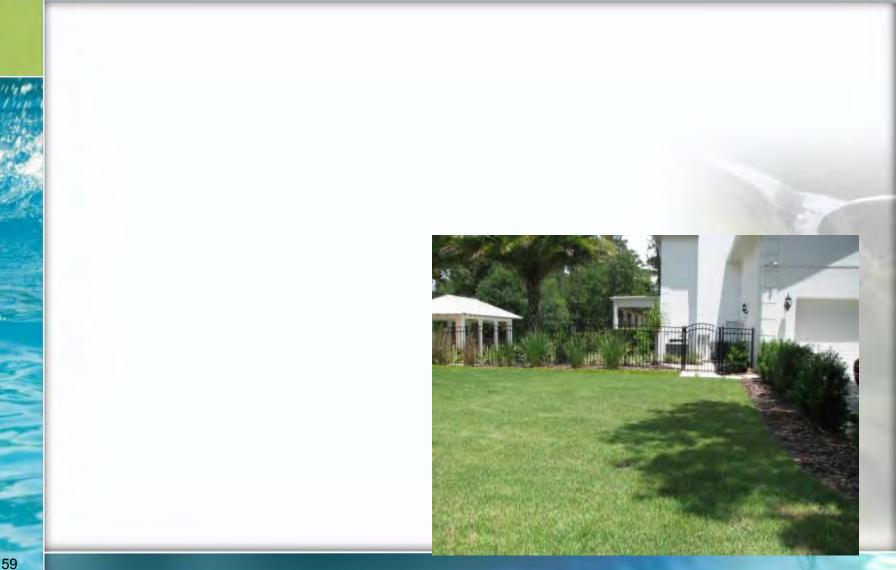


Subsurface drip irrigation of treated effluent



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Subsurface drip irrigation of treated effluent



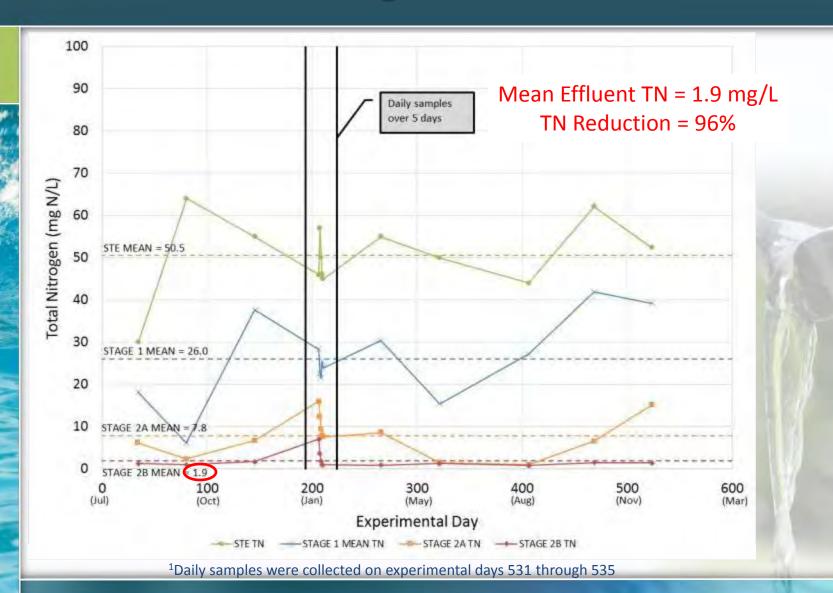
Drip irrigation controls & headworks



Completed full-scale vertically stacked in-ground PNRS with onsite reuse



System 3 Time series of nitrogen data



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System 3: Operation and maintenance

- Average energy consumption of ~1 kWh/day or 7.8 kWh/1000 gal treated
- Stage 1 biofilter no surficial biomat or clogging present
- Stage 2 biofilter reactive media shows immeasurable reduction in volume





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Summary of full scale prototype PNRS nitrogen results

	System	Design	System Description	Mean Influent TN, mg/L	Mean Effluent TN, mg/L	Mean TN Removal %
100	1	Proprietary	Stage 1 Aerocell [™] , Stage 2 Nitrex [™]	82.7	7.1	91
	2	PNRS In-tank	Stage 1 with R, dual-media Stage 2	54.7	2.5	95
	3	PNRS In-ground	Stacked Stage 1 over Stage 2a ligno with supplemental Stage 2b sulfur	50.5	1.9	96
	4	PNRS In-tank	Gravity Stage 1, dual-media Stage 2	70.1	7.4	89
	5	PNRS In-tank	Stage 1 SP and with R, dual-media Stage 2	72.1	2.1	97
	6	PNRS In-tank	Stacked Stage 1 over Stage 2a ligno with supplemental Stage 2b sulfur	66.3	12.4	81ª
	7	PNRS In-ground	In-ground stacked SP Stage 1 over Stage 2 ligno	54.9	19.1	65ª
2		^a Performance of	of systems 6 and 7 may have been significantly	y improvec	l with desig	n and

construction revisions based on lessons learned in this study.

Lignocellulosic Media Life Estimates

1	System	% Reactive Media	Media Volume, ft ³	Calculated Longevity ¹ , years	Longevity with factor of safety ² , years
IL SH	1	100%	194.8	83.8	64.5
	2	100%	126.0	107.5	82.7
	3	50%	136.5	80.8	62.2
	4	100%	126.0	21.6	16.6
	5	100%	126.0	43.6	33.5
	6	100%	67.0	39.1	30.1
	7	100%	362.0	176.2	135.5

¹ Assumptions regarding lignocellulosic media included: dry bulk density of 20 lb./ft³; 50% carbon content by weight with available carbon being approximately 50% of carbon content ² Factor of safety used was 1.3

Sulfur Media Life Estimates

				9	Study Conditio	ns	If lign	ocellulosic de	pleted
	System	% Reactive Media	Media Volume, ft ³	Mean influent NOx-N	Calculated Longevity ¹ , years	Longevity with factor of safety ² , years	Stage 1 mean influent NOx-N	Calculated Longevity ¹ , years	Longevity with factor of safety ² , years
	2	90%	32.4	0.02	N/A	N/A	16.7	194.0	149.2
	3	90%	34.7	5.8	461.2	354.8	23.9	112.2	86.3
1	4	90%	24.3	3.2	348.5	268.0	33.6	27.2	20.9
	5	90%	24.3	4.1	520.5	400.4	43.4	53.5	41.1
	6	90%	18.0	24.9	57.2	44.0	42.3	34.0	26.1

¹Assumptions regarding sulfur media included: dry bulk density of 76 lb./ft³ and influent NOx concentrations from the preceding process. In systems where lignocellulosic denitrification preceded the sulfur, low influent NO_x concentrations resulted in very long estimates of longevity. ² Factor of safety used was 1.3

PNRS Cost Analysis Tool

- User specifies nitrogen removal efficiency range, selects desired treatment process, and the tool calculates all system costs over the entire specified project life
 - Low Level (25-35% nitrogen removal efficiency)
 - Medium Level (50-70% nitrogen removal efficiency)
 - High Level (95% nitrogen removal efficiency)
- Derives the Present Worth cost
- Reported as \$/Ib nitrogen removed

2. Table of LCCA Worksheets

Worksheet	Contents
1. LCCA Structure	Two-Stage PNRS Description • Basic Model Structure • Example PNRS Systems
2. Table of LCCA Worksheets	Summary Table of LCCA Worksheets
3. Wastewater Quantity & System Parameters	Determine design flowrate • Specify conventional system parameters • Select nitrogen removal level as high, medium or low @ 95%, 50-70%, or 25-30% • Specify PNRS system parameters • Specify recurring costs • Specify net interest rate
4. PNRS Process Selection	Select specific PNRS system
5. Baseline Design & Cost	Summary of conventional system default design & cost • Summary of PNRS design and default cost
6. Baseline Design Cost Summary	Default cost summary for conventional system, for PNRS system and for total system
7. User Override Costs	User specified costs for conventional system • User specified costs for PNRS
8. LCCA: Conventional	Characteristics of conventional system • Life Cycle Cost Analysis of conventional system
9. LCCA: Total System	Characteristics of conventional system + PNRS • Life Cycle Cost Analysis of conventional system + PNRS
10. Design Data	Compilation of flow and sizing criteria, unit cost factors for materials, energy, site access and installation complexity
11. Example LCCAs	Example Life Cycle Costs







Nomenclature for LCCA Identification

Wastewater Quantity

No. of Bedrooms

Building area, square feet

Level of Treatment

What level of nitrogen removal efficiency is needed for the site?

Low conventional (25 - 35%) Medium (50 - 70%) High (95+%)

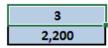
Conventional System Parameters

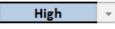
Existing system Size of existing primary treatment tank, gallons

	Size of existing pump treatment tank, ganons
	Size of existing soil treatment unit, square feet
60	il treatment unit
	Trench or bed configuration

Infiltrative surface loading rate, gal/ft ² -day
Depth to seasonal high water table (inches) at soil treatment unit







0

0

trench 0.80 60

PNRS Parameters

New OSTDS system installation or retrofit of existing system?	new	-
		-
Will a PNRS Stage 1 biofilter be used or a proprietary system (e.g. Hoot, FAST, Norweco)?	PNRS	-
What is the construction complexity? enter 1, 2 or 3		
1 Simple (new undeveloped property)	1	
2 Moderate (retrofit of existing system, easy accessibility to site)	1	Ť
3 Complex (retrofit of existing system, difficult accessibility to site)		
Is there at least an 8 foot elevation drop from the house out 60 feet in the direction of the proposed system?	no	-
		-
Standard or complex control panel?	standard	-

Construction permit fees

Enter new system conventional construction permit County fee add-on, \$

Annual operating costs

Energy Consumption	
Electrical rate, \$/kw-hour	0.100
Inspections, permit and monitoring	
Number of inspection visits per year	2
Inspection & maintenance cost per visit, \$	150
Enter PBTS operating permit County fee add-on, \$	
Number of water quality monitoring events per year	1
Water quality monitoring cost per sample event, \$	120

Maintenance costs

Primary treatment tank pump out	
Interval, years	5.0
Cost, \$	300
Media Replacement	
Stage 2 media replacement interval, years	15

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Equipment Replacement

Cost Analysis Parameters

Life Cycle Cost Analysis



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PNRS LCCA Process Selection

Processes: Stage 1&2, Stage 1 only, or Stage 2 only

Stage1&2

All blue shaded cells below must be filled in to fully specify the PNRS process

Stage 1&2 Biofilters System Selections

Stage 1 biofilter: in-tank or in-ground	Tank	
Is the Stage 2 lignocellulosic media underlying the Stage 1 media?	No	
Stage 1 biofilter mode of operation, single pass or recirculation?	Recirculation	
Stage 1 biofilter type of media, expanded clay or sand?	Expanded clay	
Stage 2 biofilter type of media: lignocellulosic, sulfur or dual media?	Dual_media	-

Stage 1 Only Selections

Stage 2 Only Selections

PNRS System Number (refers to LCCA logic)



PNRS System Summary Nitrogen Removal Efficiency High Stage 1: PNRS or proprietary **PNRS** PNRS Stage(s) Stage1&2 Stage 1: in-tank or in-ground Tank Stage 1: Single pass or recirculation Recirculation Stage 1 media type Expanded Clay Lignocellulosic disposition Tank Dual: Ligno & sulfur Stage 2 media type

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LCCA PNRS Output

Worksheet

- LCCA Structure л, Table of LCCA Worksheets 2.
- З. WW Quantity & System Parameters
- 4. PNRS Process Selection
- 5, Baseline Design & Cost
- 6. Baseline Design Cost Summary User Override Costs 7.
- 8. LCCA Conventional
- 9. LCCA Total System
- 10. Design Data
- 11 Example LCCAs

9. LCCA Total System

Installed Capital Cost Present Worth (2015 dollars) Installed Lagital Cost Engineering Design & Construction Permit Operation & Maintenanz Dompliants.

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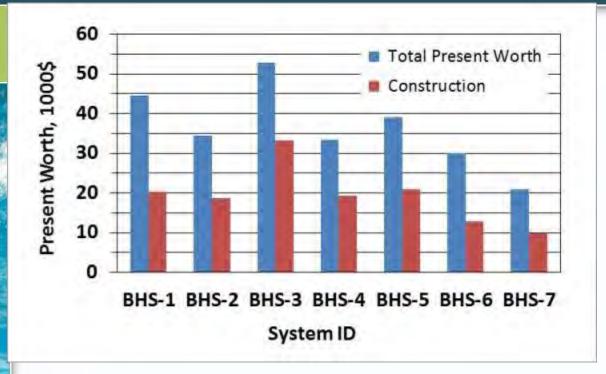
-Oni Asterna Mint. Same Procontained and produced and the

	1.1	Life Cycle Cost Calculation	ns	Life Cyc	le Cost			Installed 0	Capital Cost	8	
Conventional System Sun	imarg		1.14	Carbleom	Prásont Warth,\$	Uniform Annual Cart, \$	×af Tasar Life Oycle Cart	Installation Costltom	Prozent Warkh, \$	Uniform Annual Cart, \$	⊘of Inrtallatio Cort
No. of Bodraams	3	Project Life (PL), years	30	Conventional System Installation				Tankage	6,009.29	268.31	
Building area, rquare feet	2200 60	InterestRate (IR), 2	2.000	Primary treatment tank Pump tank	1,400.00	62.51	4.5	Sail Troatmont Unit Preprintery Steep 1 System	2,625.00	117.21	
Dopth to so aronal high water table (incher)		and the second s					0.0		0,00	0.00	
Now OSTDS installation for rotrofit of oxisting systom	Neu.	Primary tankpump but interval (TI), years	5.0	Canventionalsystempump	0.00	0.00	0.0	Modia	2,226,78	99.43	13.
Dorign wartowator flow, gallantday	300	Pump out analyziz life (PL), years	25.0	Spiltreatmentunit	2,625.00	117.21	8.4	Pump(r)	250,00	11,16	3.
				Subtotal Conventional	4,025.00	179.72	12.8	CantralPanel	\$75.00	39.07	
Be neer presside Generational sarts have t	**************************************	StageZmediareplacementinterval(MI),years	15.0	Propriotary Stage 1system	0.00	0.00	910	Mire. Appurtonance	1,693.00	75.59	10
			1	PNBSInstallation				Pipina	289.60	12.93	1
PNRS System Summa		Stage 2 modia surt analyziz life (ML), yearz	15.0	Tankago	4,609.29	205.80	14.7	Drip Dirporral Unit Camploto (cantral panol; valuer, tubing, etc.)	0.00	0,00	Ū.
		termine and the second s	-	Madia	2,226.78	99.43	7,1	Liner	0.00	0.00	0
PNRSSystem	*	Equipment replacement internal (EI), years	10.0	PNRSPump	250.00	11.16	0.8	Contractor Fee	2,500.00	111.62	15.
Stage 1: PNRS or proprietory	PNRS	Equipment replacement analysis life (EL), years	20.0	Control Panel	\$75.00	39.07	2.*	Tatal Systèm	16,468.67	735.32	100.
PNRSStage(r)	Stage 182	1 mm		Piping	289.60	12.93	0.9				
Stage fin-tank or in-ground	Tank	GampaundInterertFactors		Mirc, Appurtanance	1,693.00	75.59	5.4	Life Cycle Cost			
Stage Isingle pass as recirculation	Rocirculation,	PIA PLNR	22.396	Stage 1Drip Dispersal System Complete (control panel, valves,	0.00	0.00	0.0	Cartitom	Prozent Warth,	Uniform Annual	ZafTata LifeCycl
StageImediatype	Expanded Glay	A/P PL//P	0.04465		0.00	0.00	0.0	Installed Capital Cast	16,468.67	Cart.\$ 735.32	Cart 52.
Ligno-disparition	Tank	A/F TI	0.19216	Contractor Foo	2,500.00	111.62	\$.0	Engineering Derign & Construction Permit	1,375.00	61.39	a.
Stage 2 media type	Dual:Ligna &salfur	PAPL	19.523	Subtatal	12,443.67	555.61	39.7	Operation®Maintenance	9,691.56	432.73	30.
Construction Complexity	Simple	G/F (H)	0.05783	Total System Installation	16,468.67	735.32	52,5	Compliance	3,807.40	179.00	12:
Local of nitrugon romuval officioney pravided by syste	n Hial	PYA ML	12.849					Tatal	31,342.63	1,399.45	100.
0.000 000000000000000000000000000000000		AIF EI	0,09133	Engineering Derign & Courtrue	tion Permit						
Be and searcide PHRS carts have been spe	cified	P/A EL	16.351	Construction permit	375.00	16.74	1.2	\$/Ib nitrugon romayod	40.71	54.52	
		Nitrogen Romoval		Engineering derign feer Operation and Maintenance	1,000.00	44.65	3.2				
		Marr laadingt yoar, lbr,	27.0	Annual onergy cart	736.23	32.\$7	2.3				
		Bombyalofficioncy, 2	95.0	Annual inspection & maintenance	6,718.94	300.00	21.4				
		Mari romovali yoar, ibr.	25.66	Primary tank pump but Stage 2 media replacement	1,125.48	50.25 32.93	3.6				
				Equipment replacement	373.33	16.67	1.2				
				Subtatal	9,691.56	432.73	30.9				
100000000000000000000000000000000000000	10.000			Campliance							
Developed by: HAZEN AND	SAWVER	AFT		Operating permit fee	1,119.82.	50.00	3.6				
and the state of the state of the	THEFT PRINT	ALI		Water quality monitoring	2,687.57	120.00	3.6				
A REAL PROPERTY AND A REAL				Subtotal	3,807.40	170.00	12,1				

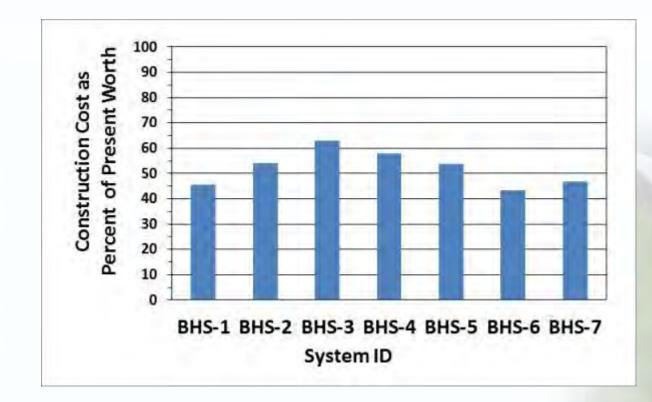
Summary of PNRS Construction Cost

		Total Sys	stem Costs		
System	System Description	Total PW, \$	Total Construction Cost, \$	Conv. Component Construction Cost, \$	PNRS Component Construction Cost, \$
BHS-1	Proprietary	44,533	20,349	5,225	15,124
BHS-2	In-tank	34,545	18,697	2,576	16,121
BHS-3	In-ground	52,763	33,155	10,734	22,421
BHS-4	In-tank	33,373	19,350	3,171	16,180
BHS-5	In-tank	39,003	20,920	0	20,920
BHS-6	In-tank	29,926	12,926	0	12,926
BHS-7	In-ground	20,940	9,800	0	9,800

PNRS LCCA Construction Costs

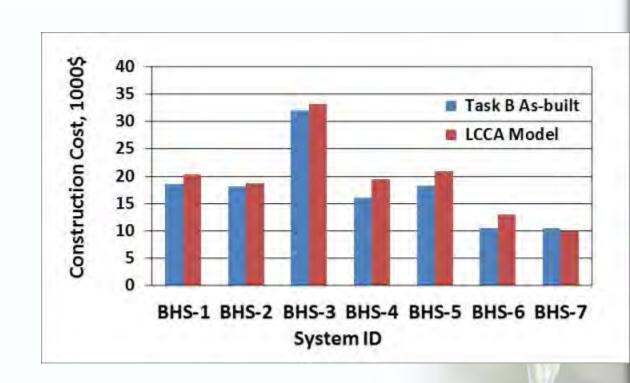


PNRS LCCA Construction Costs

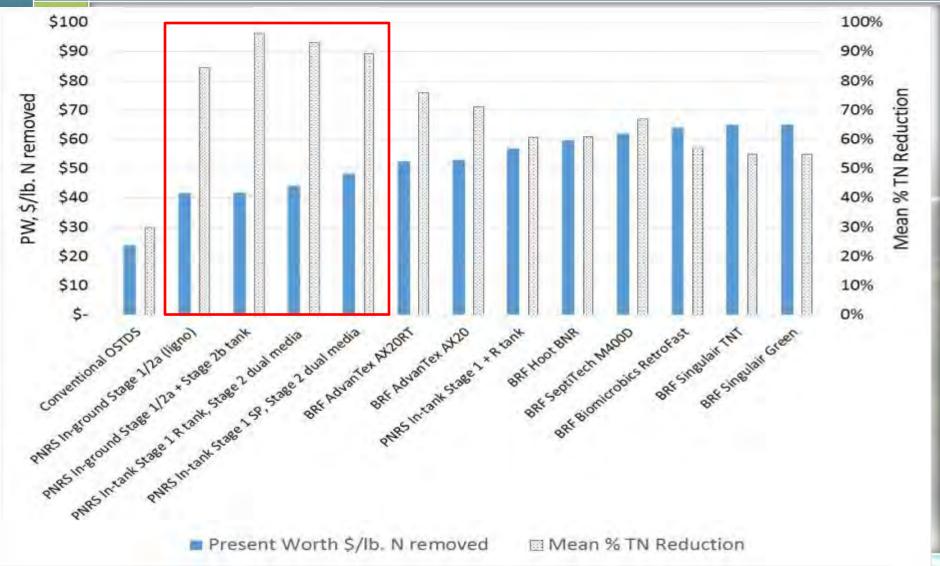


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PNRS LCCA Construction Costs



Comparison of PNRS LCCA to Other Studies (Maryland BRF)



Task B Recommendations: Treatment Process – 3 Levels of Treatment

- Low level onsite wastewater nitrogen removal
 - TN reductions (from STE) of 25-35% prior to GW
 - Compliant conventional system with STU meets this level of treatment
- Medium level onsite wastewater nitrogen removal
 - TN reductions (from STE) of 50 70% prior to GW
 - Stage 1 PNRS w recirculation or in-ground Stage1/Stage 2 PNRS followed by STU
- High level onsite wastewater nitrogen removal
 - TN reductions of 95% prior to GW
 - Numerous 2-stage PNRS configurations from study followed by STU

Task B Recommendations: Technical Recommendations

- Long term monitoring of PNRS is needed to evaluate reliability and life
- PNRS specific tanks, equipment, media, appurtenances are needed prior to widespread implementation
- Detailed design criteria and designs should be developed for several standardized PNRS
 - PNRS specifications should be established for all materials and methods
 - Tanks, lids & covers, liners, media, pipe, controls, process controls, operations

Recommendations: PNRS Implementation

- Establish uniform guidance for PNRS regulation and permitting, streamline permitting requirements.
- Establish uniform requirements for PNRS inspection, operation and maintenance
- Establish uniform requirements for PNRS performance monitoring
 - Implement technology transfer and training on PNRS implementation
- Establish sufficient FDOH staffing for PNRS implementation, including wastewater engineering staff



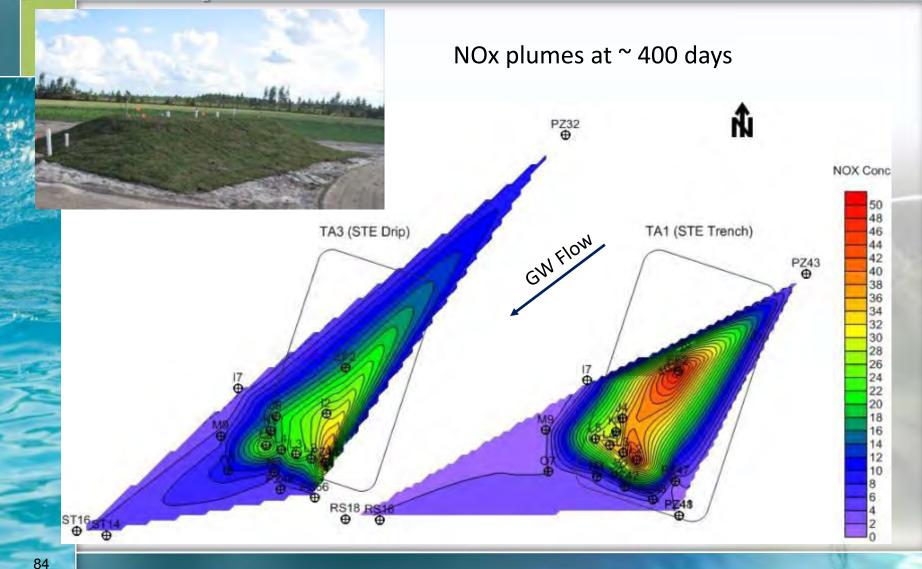


Task C: Soil and Groundwater Monitoring

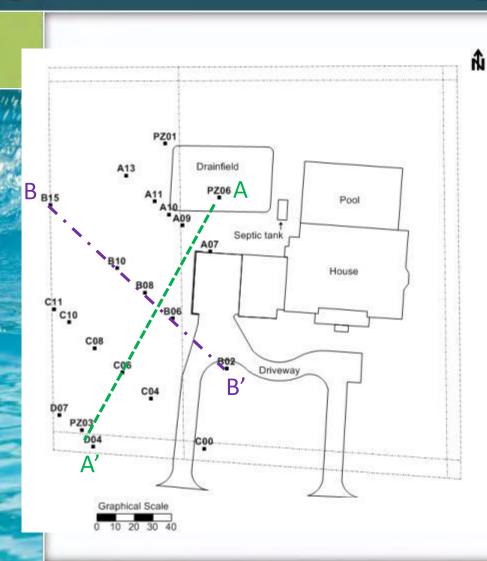
Task C Components

- Literature review to evaluate nitrogen fate and transport in saturated and unsaturated soils
- Developed the soil and groundwater (S&GW) research test facility
- Conducted soil and groundwater monitoring at test facility
- Conducted 3 tracer tests at the S&GW test facility
- Groundwater monitoring at 4 single family residences

Soil and Groundwater Test Facility: N transport studies



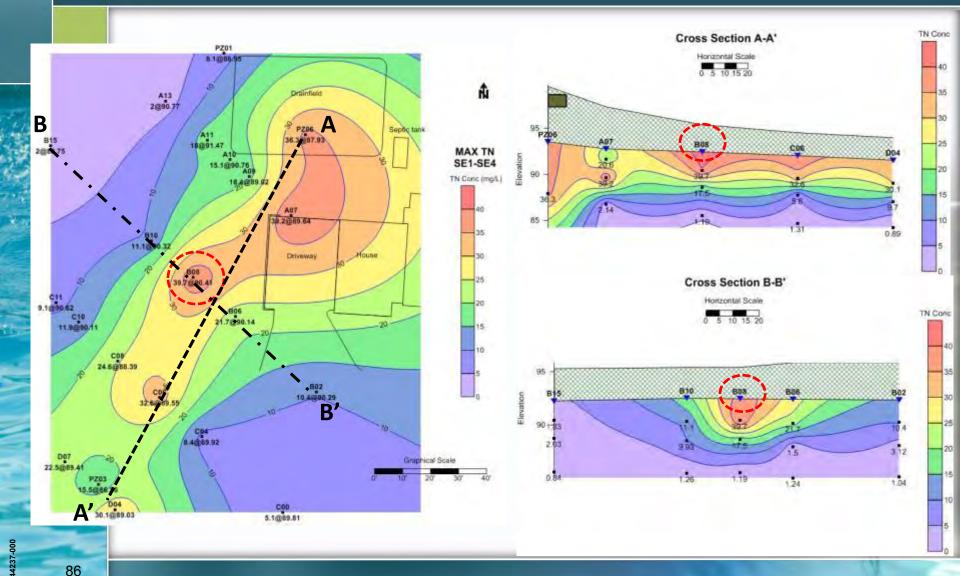
Home site (conventional system) groundwater monitoring network



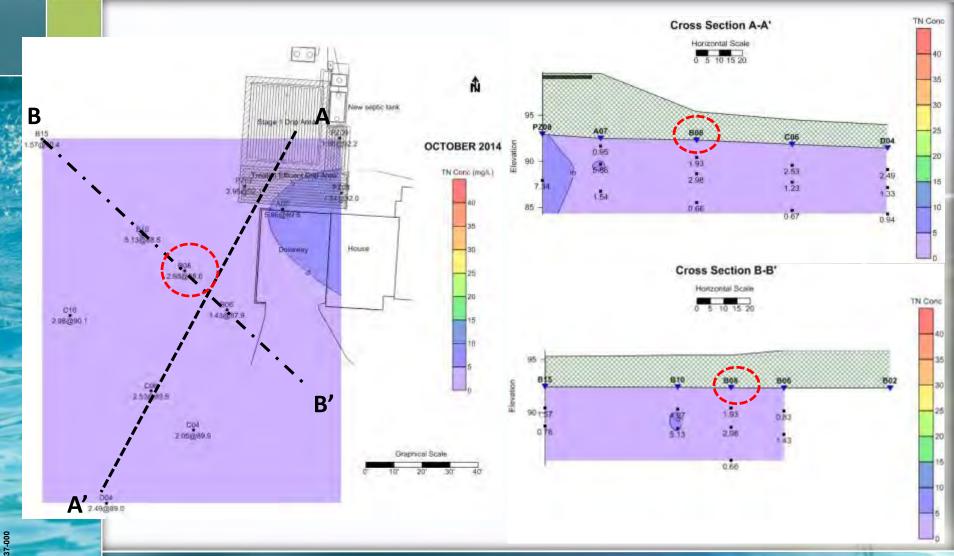




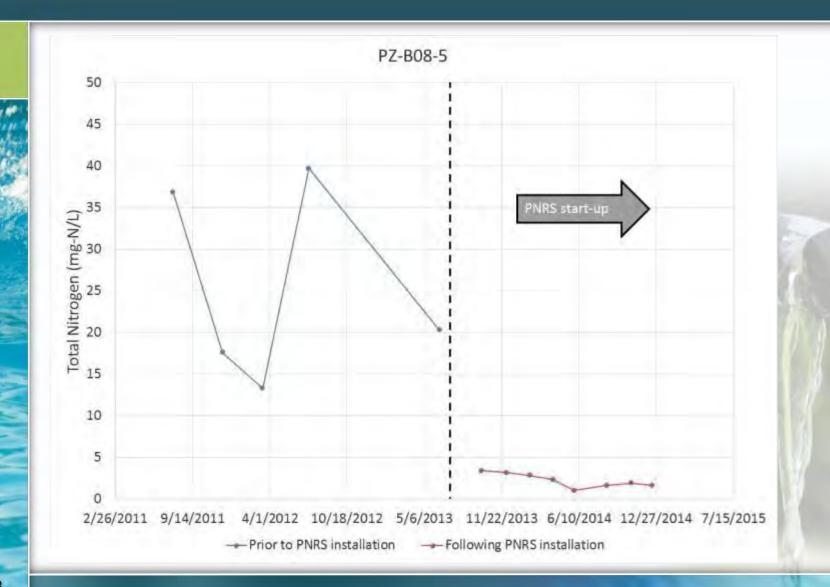
Groundwater monitoring results



Groundwater monitoring: After PNRS installation (System 3)



Most impacted groundwater well Total nitrogen time series







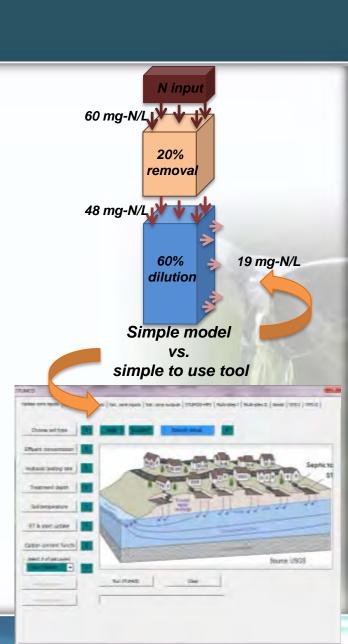
Task D: Nitrogen Fate and Transport Modeling and Tool Development

Task D Components

- Literature review to evaluate nitrogen fate and transport models
- Simple soil tool for vadose zone N transport
- Development of Florida specific vadose zone fate and transport model (STUMOD-FL)
 - Development of saturated zone fate and transport model (HPS)
- Development of combined vadose and saturated zone fate and transport model (STUMOD-FL-HPS)
- Incorporation of multiple OWTS inputs
- Sensitivity analysis
- Uncertainty analysis

Task D - Overview

- Provide a simple to use tool for assessment of OWTS performance and impact to groundwater
 - Literature Review
 - Simple tool
 - Simple to use spreadsheet model, STUMOD-FL-HPS



Task D – Deliverables

- Simple tools
 - tables of selected Florida conditions
 - Outcomes
 - white paper discussing relative differences in nitrogen behavior based on various conditions
 - 64 numerical model simulations (HYDRUS-2D)
 - corroboration to field data
 - look-up tables



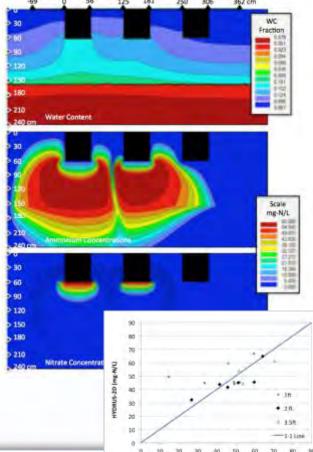
 Scenario 61
 trench, unequal distribution

 Soil Type:
 0-160 cm (0-5.25 ft) less permeable sand; 160-244 cm (5.25-8 ft) sandy clay loan

 Loading Rate:
 5.35, 2.67, 0 cm/d (1.31, 0.65, 0 epd/ft²)

 Effuent Nitrogen:
 60 mg·N/L as NH,

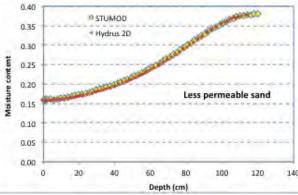
 Depth to Water Table:
 183 cm (6 ft) below the infiltrative surface

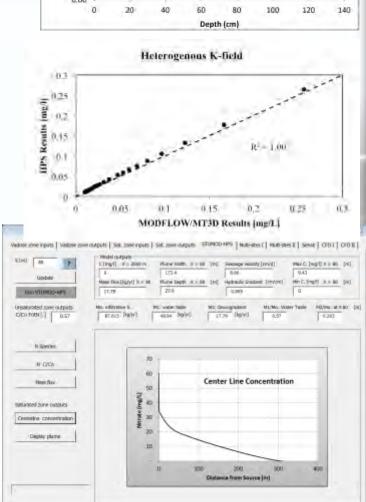


Field data (mg-N/I

Task D - Deliverables

- Complex soil-aquifer model
 - rigorous scientific principals, but simple to use
 - stand alone tool
 - Outcomes
 - STUMOD-FL-HPS
 - combined unsaturated and saturated zone model
 - corroborated to field data / validated with numerical model
 - demonstration...









Summary & Questions

FOSNRS Summary

- Multi-prong project for evaluating nitrogen reduction from onsite sewage treatment and disposal systems:
 - Treatment technology evaluation including new passive systems
 - Full scale field testing of PNRS treatment technologies
 - Monitoring of nitrogen fate and transport in subsurface
 - Modeling and planning tools to support regulatory decision making

FOSNRS Summary (cont)

- Results indicate that OSTDS are capable of achieving high levels of nitrogen reduction and can play a role in nitrogen reduction from OSTDS in sensitive watersheds
- Useful tools were developed to assist with planning and implementation of nitrogen reduction strategies for OSTDS in Florida
 - PNRS-LCCA
 - Simple Soil Tools
 - STUMOD FL
 - STUMOD FL HPS

What's left to do?

- Link the results of all FOSNRS tasks together into a final database and report.
- Link treatment, soil and groundwater tools to develop onsite wastewater nitrogen reduction best management practices (BMPs)
- Develop onsite wastewater nitrogen reduction management strategies for Florida, based on nutrient sensitivity. Watershed/water body sensitivity varies, N reduction is not needed everywhere.
- Develop detailed design criteria, performance definitions, performance boundaries, and strategy implementation guidance
- Move forward with implementation



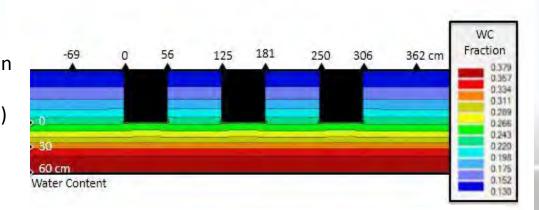


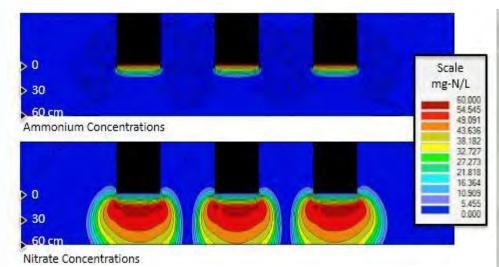
QUESTIONS ?

Damann L. Anderson, P.E., Vice President Josefin E. Hirst, P.E., Senior Principal Engineer Hazen and Sawyer Phone: 813-630-4498 e-mail: danderson@hazenandsawyer.com jhirst@hazenandsawyer.com

Hydrus 2D modeling of multiple vadose zone nitrogen fate and transport scenarios

Configuration:trench, equal distributionSoil Type:less permeable sandLoading Rate: $2.67 \text{ cm/d} (0.65 \text{ gpd/ft}^2)$ Effluent Nitrogen: $60 \text{ mg-N/L as NH}_4$ Depth to Water Table:60 cm (2 ft)



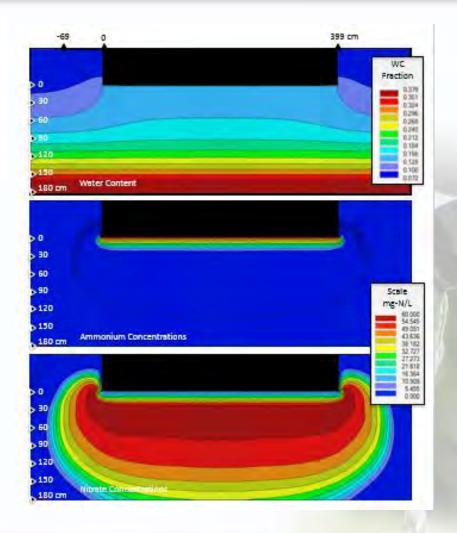


Vadose Zone Operating Conditions Modeled

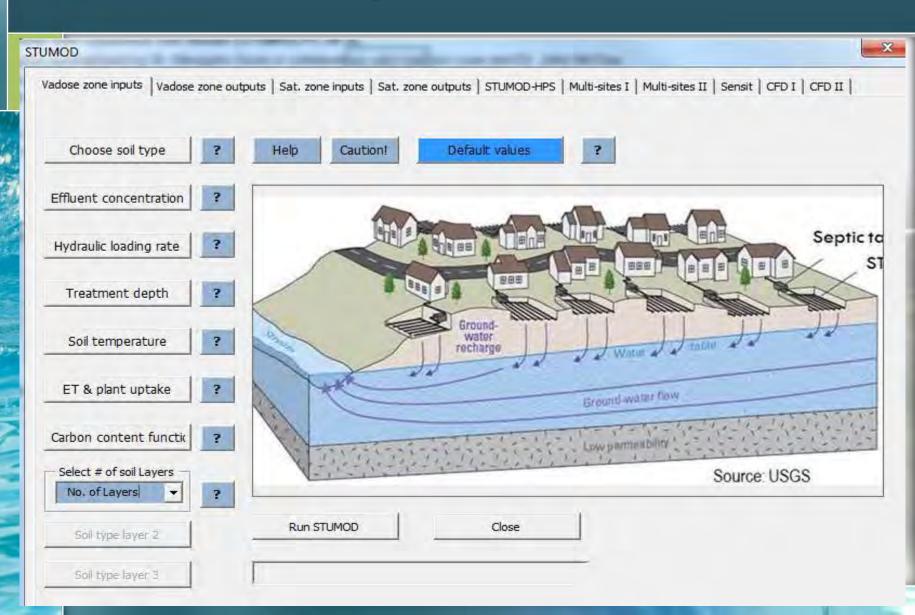
ions Simulated
distribution to each trench; nt distribution to each trench; bution to each bed; or
stribution to each bed.
e surface; e surface; e surface; or er table).

Simple Soil Tool for estimating vadose zone N transport

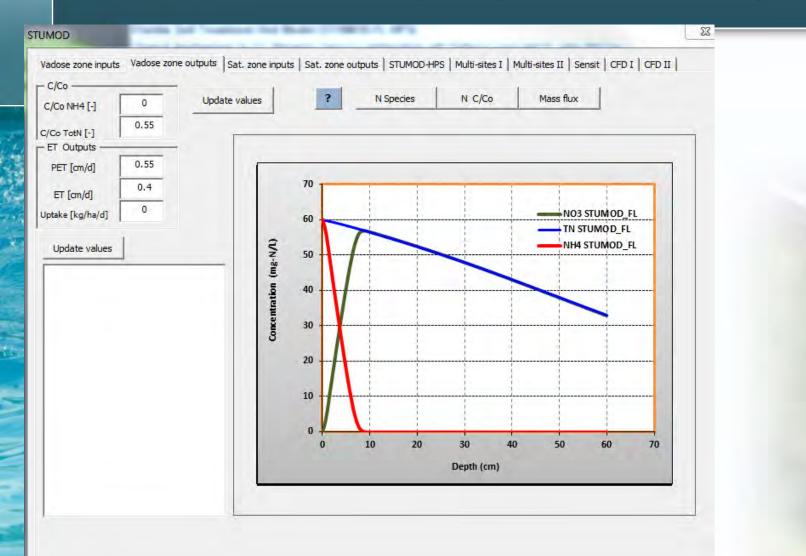
Configuration:bed, equal distributionSoil Type:less permeable sandLoading Rate:1.68 cm/d (0.41 gpd/ft²)Effluent Nitrogen:60 mg-N/L as NH4Depth to Water Table:183 cm (6 ft)



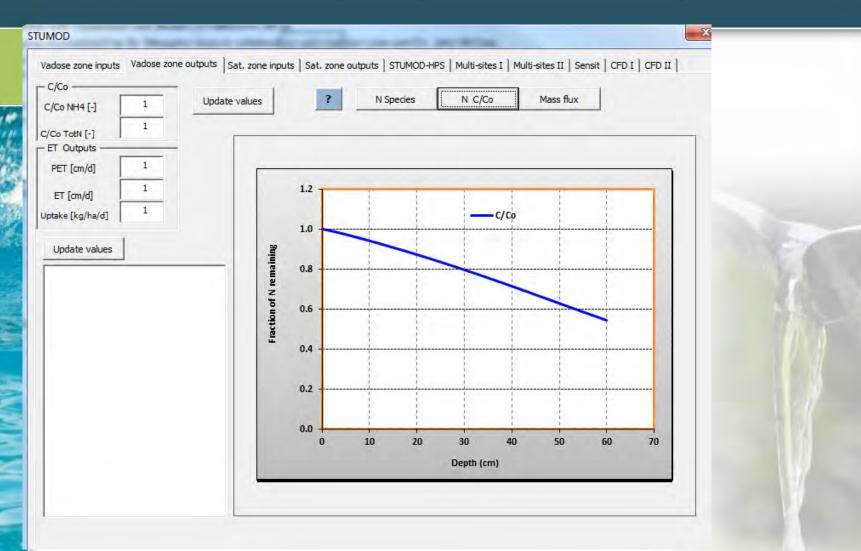
STUMOD FL: Graphical user interface



Vadose zone output (STUMOD-FL)



Vadose zone output (STUMOD-FL)



1

Vadose zone output (STUMOD-FL)

STUMOD

C/Co		. 1		1			~ [Marca A.		
C/Co NH4 [-]	1 Update va	alues	?	N	Species	N C/		Mass flux		
C/Co TotN [-]	1									
- ET Outputs										
PET [cm/d]	1	-								
ET [cm/d]	1		1.4	1	1	1	1	1		
Uptake [kg/ha/d]	1		1.2	_		-	— Mass Fl	ux TN		
Update values		lay-1)	1.0		-	-				
		Mass Flux (g m-2 day-1)	0.8				/			
		iss Flux	0.6						1	
			0.4							
			0.2							
			0.0	1	1	Î	1	1	1	_
			0	10	20	30 Depth	40	50	60	70

Saturated zone (HPS) inputs

Y, Z Plume Cross Section Specifiy X [m] 90
values

-

Saturated zone (HPS) outputs

	Outputs Outputs /I] X = 2000 m Plume Width X = 15 [m] Seepage Velocity [cm/d] Max C. [mg/l] X = 15 [m] 195 8.66 1.87	
1	$ _{lux} [kg/yr] \times = 15$ [m] Plume Depth $\times = 15$ [m] Hydraulic Gradient [cm/cm] Min C. [mg/l] $\times = 15$ [m]	
M1: water	r table M2: Downgradient M2/M1: at X = [m] [kg/yr] [kg/yr] [m]	
	60	
Display plume ?	Center Line Concentration	

Saturated zone (HPS) outputs

	Model Outputs C [mg/l] X = 2000 m	Sat. zone outputs STUMOD-HPS	Seepage Velocity [cm/d]	Max C. [mg/l] X = 15 [m
	0	195	8.66	1.87
Display values	Mass Flux [kg/yr] X = 15	[m] Plume Depth X = 15 [m]	, Hydraulic Gradient [cm/cm] Min C. [mg/l] × = 15 [m]
	1.57	30.8	0.005	0
	M1: water table [kg/yr]	M2: Downgradient [kg/yr]	M2/M1: at X = [m]	1
	-	Plume Cross Se	ction	
Display plume	E 1			Legend (mg/) 1.9E+00 1.8E+00 1.4E+00 1.3E+00
	pth, 31 m			1.9E+00 1.6E+00 1.4E+00 1.3E+00 1.1E+00
	Depth, 31 m			1.9E+00 1.8E+00 1.4E+00 1.3E+00
	Depth, 31 m			1.9E+00 1.6E+00 1.4E+00 1.3E+00 1.1E+00 9.8E-01 8.4E-01 7.3E-01
	Depth, 31 m			1.9E+00 1.6E+00 1.4E+00 1.3E+00 1.1E+00 9.6E-01 8.4E-01
	Depth, 31 m			1.9E+00 1.8E+00 1.4E+00 1.3E+00 1.1E+00 9.8E-01 8.4E-01 7.3E-01 6.4E-01